

1. A Bingham plastic flows if $\tau_{\text{total}}|_{r=R} \geq \tau_0$ (BSL1 Ex.

2.3-2). In other words,

$$\left(\frac{p_D - p_L}{2L}\right) R \geq \tau_0$$

[see note on next page]
(I)

What is $\Delta p = (p_D - p_L)$?

$$p_D = 10^5 \text{ Pa} + \rho g(0.1) \quad (\text{entrance } 10 \text{ cm below top of manometer})$$

$$p_L = \text{unknown}$$

$$\Delta p = p_D - p_L - \rho g(0.3) \quad - \text{flow goes up, against gravity, } 0.3 \text{ m}$$

$$= 10^5 - p_L - \rho g(0.3) \quad (\text{Note entrance } (p_D) \text{ is at bottom of tube})$$

$$(\text{From Eq I}) (10^5 - p_L - \rho g(0.3)) \geq \tau_0 \frac{2L}{R}$$

$$p_L \leq 10^5 - \rho g(0.3) - \tau_0 \frac{2L}{R}$$

$$\leq 10^5 - (910)(9.82)(0.3) - 100 \left(\frac{2(0.3)}{0.002}\right)$$

$$\leq 10^5 - 1787 \quad - 3 \cdot 10^4$$

$$\leq 6.82 \cdot 10^4 \quad (\text{almost } 1/3 \text{ bar vacuum})$$

(Note that μ_0 is irrelevant to the onset of flow.)

2. a) We don't know v , so we don't know Re , τ_{total} + error:

$$f = \frac{4}{3} g D \frac{1}{\sqrt{g}} \frac{\rho_s - \rho}{\rho} \quad (\text{BSL1 Eq. 6.1-7})$$

$$= \frac{4}{3} (9.82) 10^{-4} \frac{1}{\sqrt{2}} \left(\frac{2500 - 1000}{1000}\right) = \frac{0.001964}{\sqrt{2}}$$

$$Re = \frac{\rho v r}{\mu} = \frac{10^{-4} v 1000}{0.001} = 100 v$$

I would guess with a small particle, Re is small.

$$\text{Guess } v = 0.01 \text{ m/s}; Re = 1; f \approx 30 \rightarrow v = 0.0031$$

$$Re = 0.8 \quad \sim 35 \quad v = 0.0075 \text{ m/s}$$

0.75 can't read difference. Done

$$b) \text{ Now } f = \frac{0.000982}{\sqrt{2}}; Re = 50 v$$

$$\text{Guess } v = 0.002 \text{ m/s}; Re = 0.2 \quad f \approx 130 \rightarrow v = 0.0027$$

$$0.27$$

$$0.0031$$

Slower velocity for smaller grains \rightarrow longer time

to settle. Smaller grains are layered on larger grains.

\uparrow In a turbidite

3. There are two differences from BSL1 Sect. 2.:

- Different BC at $x = \delta$; instead, $v = v \neq 0$ at $x = \delta$
- viscosity not constant.

Which change affects derivation first?

The integration of Eq. 2.2-12 to obtain Eq. 2.2-13 assumes μ is constant. This comes before the B.C. at $x = \delta$ (Eq. 2.2-15).

Therefore, the last eq. that can be used directly is

Eq. 2.2-13

Depending on whether you interpret ^{symbol} μ as necessarily a constant, one might say eq. 2.2-11 is the last eq. that applies. I accepted any answer between 2.2-11 and 2.2-13. By eq. 2.2-14, though, the integration has been done assuming μ is a constant.

Note on solution to problem 1:

Because we are interested in the onset of flow, you don't need the equation for U_z (BSL1 2.3-25+26) or Q (BSL1 2.3-10). Moreover, note that eq. 2.3-25 applies only for $r > r_0$. At the onset of flow, $r_0 = R$, and $T_r = T_e$. Either way, one is driven back to the condition that $T_{rz}|_{r=R} = 0$.

4. a) A sudden constriction and kinetic energy are involved.

Use macro mech E balance (BSL I Eq. 7.5-12)

Surface "1" just upstream of tube; "2" at outlet.

$$\frac{1}{2}(v_2^2 - v_1^2) = \frac{1}{2}v^2$$

$$g(h_2 - h_1) = 0.2(9.82)$$

$$\frac{p_2 - p_1}{\rho} = \frac{10^5 - 2.10^5}{1000} = -100$$

no work in or out

fittings: one sudden constriction.

$$\frac{1}{2}v^2(0.45)$$

$$\text{friction along tube: } 2v^2 \frac{0.2}{0.005} f \quad (\text{III})$$

Putting it together:

$$\frac{1}{2}v^2 + 1.96 - 100 = -2v^2 40 f(\text{Re}) - 0.225v^2$$

$$v^2 \left(\frac{1}{2} + 80f + 0.225 \right) = 98.04 \quad (\text{II})$$

Need to solve by trial + error. $\text{Re} = \frac{Dv\rho}{\mu} = \frac{0.005v(1000)}{0.001} \approx 5000v$

Guess $v = 1 \text{ m/s}$; $\frac{K}{D} = \frac{0.02}{5} = 0.004$, $\text{Re} = 5000$, $f \approx 0.01$ (Fig 6.7-2)

$$v^2 (0.725 + 80(0.01)) = 98.04 \rightarrow v = 8.0 \text{ m/s}$$

$$\text{Re} = 4.0 \cdot 10^4 \quad f \approx (0.0082) \rightarrow v = 8.4 \text{ m/s}$$

$\text{Re} = 4.2 \cdot 10^4$ ≈ 0.0082 again. Can't tell difference. Done

b) if D increases, the only term in Eq. II to change is the friction-factor term, Eq. (III). It gets smaller^{er}, which makes the bracketed term in Eq. II smaller. That means v increases. He should use the largest tube dia. practical, as long as his tank can continue to supply water at constant pressure.

* in 2 ways: first, at fixed roughness factor $\frac{K}{D}$, f decreases a bit as Re increases. More important, $\frac{K}{D} \downarrow$ as $D \uparrow$, so $f \downarrow$.

Why does this seem to contradict experience? If the ability to supply water at fixed p were limited (in other words, fixed D , not fixed p), then a narrower tube would be better.